

Flash Point Estimation

Short Introduction and Tutorial

DDBSP - Dortmund Data Bank Software Package



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1 Introduction

This software calculates flash points of flammable liquid mixtures by the UNIFAC based methods “original UNIFAC”¹, “modified UNIFAC (Dortmund)”² and “NIST modified UNIFAC”³. All methods are delivered with the latest published parameters.

The algorithm to calculate the flash points is described in a scientific paper⁴ from 1982. The basic procedure is that from known pure component properties (flash point and heat of combustion) the real behavior of the mixture is estimated by the activity coefficients which are obtained from the predictive group contribution models orig. UNIFAC and modified UNIFAC (Dortmund). Additional needed parameters are Antoine coefficients for the calculation of the saturated vapor pressures of pure components.

1.1 Theoretical Background

The flash point temperature of a pure combustible component is the temperature T_F for which the saturated pressure is equal to the lower flammability limit:

$$\frac{P_i^S}{L_i} = 1 \text{ or } P_i^S = L_i$$

with

P_i^S Saturated vapor pressure of component i

L_i Lower flammability limit of component i

For mixtures, this relation can be extended to

$$\sum_{i=1}^N \frac{P_i}{L_i} = 1$$

with

N Number of components

P_i Partial pressure of component i in a vapor-air mixture in equilibrium

L_i Partial pressure in a vapor-air mixture of component i corresponding to the lower flammability limit of the pure component.

The temperature dependence of the lower flammability limit is estimated by the function

$$L_i(t) = L_i(25^\circ\text{C}) - 0.182 \frac{t - 25}{H_{ci}}$$

with

¹Wittig R., Lohmann J., Gmehling J., "Vapor-Liquid Equilibria by UNIFAC Group Contribution. 6. Revision and Extension", Ind.Eng.Chem.Res., 42(1), 183-188, 2003

²Jakob A., Grensemann H., Lohmann J., Gmehling J., "Further Development of Modified UNIFAC (Dortmund): Revision and Extension 5", Ind.Eng.Chem.Res., 45(23), 7924-7933, 2006

³Constantinescu D., Gmehling J., "Further Development of Modified UNIFAC (Dortmund): Revision and Extension 6", J.Chem.Eng.Data, 61(8), 2738-2748, 2016.

⁴Gmehling J., Rasmussen P., "Flash Points of Flammable Liquid Mixtures Using UNIFAC.", Ind.Eng.Chem. Fundam., 21(2), 186-188, 1982

$L_i(t)$	Lower flammability limit at temperature t in °C of component i
$L_i(25^\circ\text{C})$	Lower flammability limit at temperature 25 °C (tabulated, stored) of component i
H_{ci}	Heat of combustion of component i in kJ/mol typically.

The partial pressures at vapor-liquid equilibrium conditions P_i can be calculated by

$$P_i = x_i \gamma_i P_i^S$$

when the vapor-air mixture behaves as an ideal gas.

x_i	Mole fraction of component i
γ_i	Activity coefficient of component i at a given temperature
P_i^S	Saturated vapor pressure of component i at a given temperature

The activity coefficients γ_i are calculated by UNIFAC, the saturated vapor pressure of the pure components by the Antoine equation.

The flash point temperature T_F can now be calculated by iterating this equation to fulfill the condition

$$\sum_{i=1}^N \frac{P_i}{L_i} = 1.$$

1.1.1 Inert Components

Inert (non-combustible) components like water in the mixture reduce the partial pressures P_i of the combustible components. This leads to a higher flash point temperature because the vapor pressure needed for the ignition of the combustible components is obtained at higher temperatures. Additionally, inert components change the activity coefficients of the combustible components leading also to different partial pressures.

1.2 Available Parameters

The software includes

- flash point temperatures for 1229 components
- heats of combustion for 1710 components
- flash point temperatures and heats of combustion for 453 components (both needed values are available)
- Antoine coefficients for approx. 6250 components
- original UNIFAC group assignments for approx. 26,750 components
- mod. UNIFAC (Dortmund) group assignments for approx. 30,850 components.

Flash points and heats of combustion can be entered directly in the program for every component. Antoine coefficients and group assignments are directly taken from data files and can be altered or added for private components.

2 Using the Program

The graphical user interface contains four major parts:

- A menu bar
- Several controls for the component management
- A panel with controls for the calculation, model selection, and data display
- A grid for the results

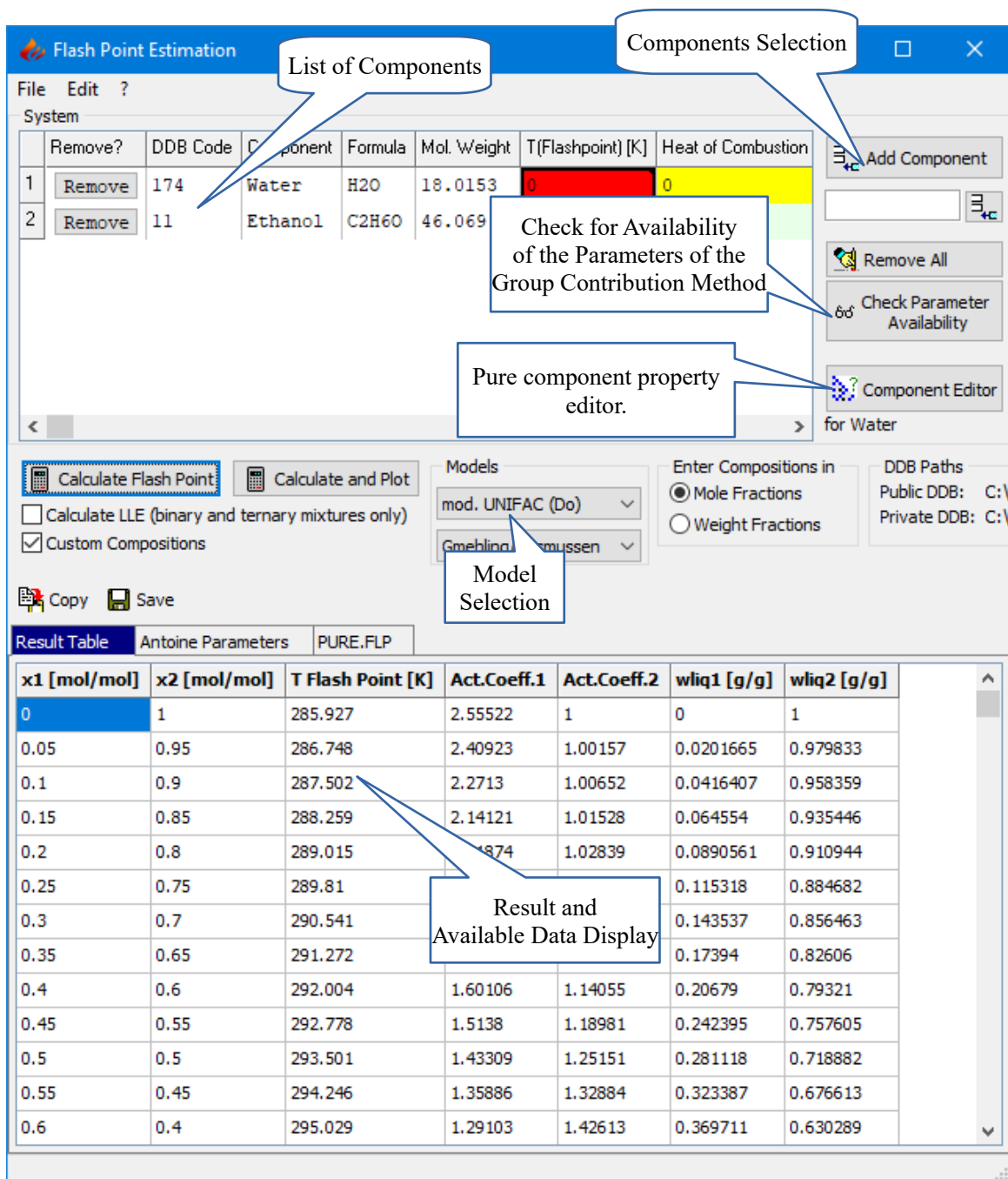


Figure 1: Graphical user interface

The result grid itself has a tool button bar which allows copying and saving the grid content.

2.1 Menu bar

- The button “Exit” in the file menu closes the program.
- The edit menu contains the following selections
 - “Component Editor” executes the separate program for editing basic component data.
 - “Interaction Parameters” execute the program that displays the interaction and other parameters for the models.
 - “DDB Configuration” executes the program for the DDB configurations (paths and settings etc.).
- The “?” contains a link to the manual the “About” button which displays the accordant dialog.

2.2 Component Management

The component grid shows the DDB number, a typical name, the empirical formula, the molecular weight, flash point and heat of combustion of the different components.

This component management uses the standard list of components in the Dortmund Data Bank. The component selection is done in the component selection program which is described in a separate PDF (see “ComponentManagement.pdf”).

The “Add Component” button calls the component selection program:

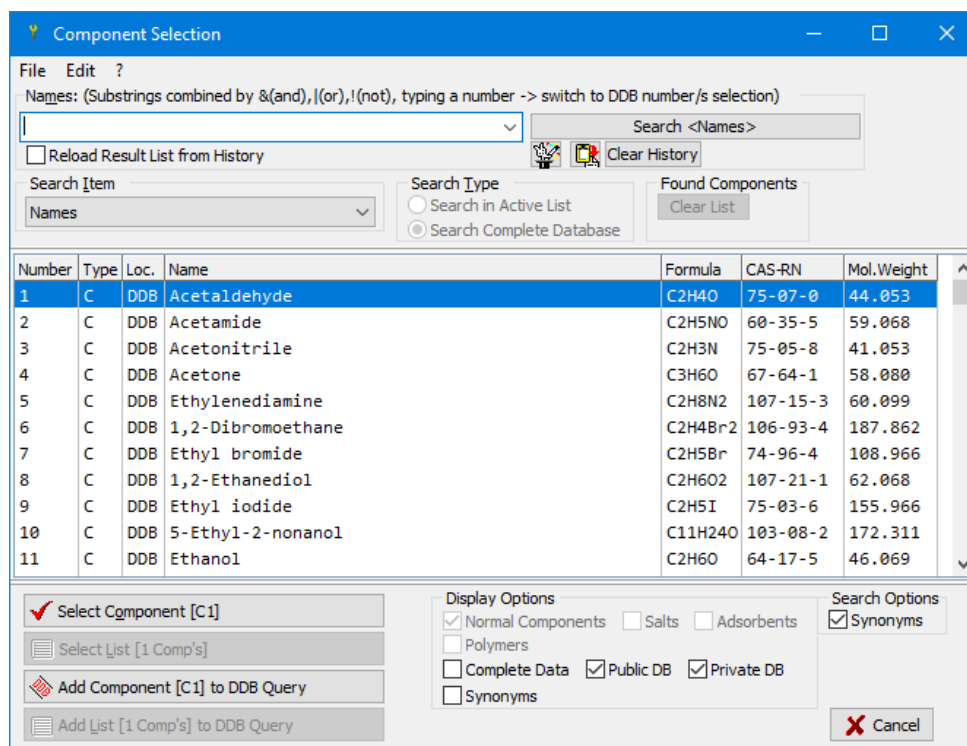


Figure 2: Component selection dialog.

Here it is possible to search the complete component file of the Dortmund Data Bank by names, formula, etc. The edit field below the “Add Component” button allows the input of components by DDB numbers directly. This is useful after some experience with the DDB component list and the knowledge of the DDB numbers of the main components.

2.2.1 Adding Missing Flash Point Data

	Remove?	DDB Code	Component	Formula	Mol. Weight	T(Flashpoint) [K]	Heat of Combustion [kJ/mol]
1	<input type="button" value="Remove"/>	11	Ethanol	C ₂ H ₆ O	46.069	285.93	-1368.5
2	<input type="button" value="Remove"/>	21	Ethyl acetate	C ₄ H ₈ O ₂	88.1063	268.71	-2250.41

The component grid displays information about

- The DDB code number
- A typical component name
- The empirical formula
- The molecular weight
- Flash point temperature in [K]
- Heat of combustion in [kJ/mol]

The last both cells are editable and allow entering new values for both the pure components flash point temperature and the heat of combustion. Fragmentation and Antoine coefficients for private components can be changed / fitted by pressing the “Component Editor” button. A new window pops up and shows the pure component properties of the marked component:

Figure 3: View and edit pure component properties.

2.2.2 Inert Components

Inert components are added like normal components. Inert components are recognized by the missing flash point temperature and heat of combustion.

2.3 Check Interaction Parameter Availability

This function checks if the activity coefficients of the defined mixture can be calculated with the group contribution models. The dialog has two pages – the first with an overview if the calculation is possible or not

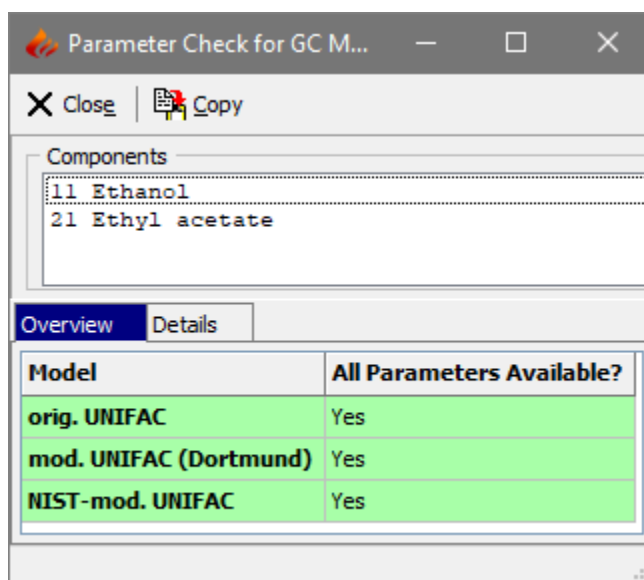


Figure 4: Check for available interaction parameters and group assignments.

and the second page with details about the group assignments (sub and main groups) and the interaction parameters.

UNIFAC

```
Component      11: Ethanol
                Subgroups:  1 (CH3   )   2 (CH2   )   14 (OH    )
Component      21: Ethyl acetate
                Subgroups:  1 (CH3   )   2 (CH2   )   21 (CH3COO )
```

List of Main Groups

```
Maingroups:   1 (CH2   )   5 (OH    )   11 (CCOO  )
```

Interaction parameters

```
 1 - 5: 1 parameter/s (CH2   / OH    )
 1 - 11: 1 parameter/s (CH2   / CCOO  )
 5 - 11: 1 parameter/s (OH    / CCOO  )
```

System has all parameters available.

mod. UNIFAC (Dortmund)

```
Component      11: Ethanol
                Subgroups:  1 (CH3   )   2 (CH2   )   14 (OH (P) )
Component      21: Ethyl acetate
                Subgroups:  1 (CH3   )   2 (CH2   )   21 (CH3COO )
```


List of Main Groups

Maingroups: 1 (CH2) 5 (OH) 11 (CCOO)

Interaction parameters

1 - 5: 3 parameter/s (CH2 / OH)
1 - 11: 3 parameter/s (CH2 / CCOO)
5 - 11: 3 parameter/s (OH / CCOO)

System has all parameters available.

NIST-mod. UNIFAC

Component 11: Ethanol
Subgroups: 1 (CH3) 2 (CH2) 14 (OH prim)
Component 21: Ethyl acetate
Subgroups: 1 (CH3) 2 (CH2) 21 (CH3COO)

List of Main Groups

Maingroups: 1 (CH2) 5 (OH) 11 (CCOO)

Interaction parameters

1 - 5: 3 parameter/s (CH2 / OH)
1 - 11: 3 parameter/s (CH2 / CCOO)
5 - 11: 3 parameter/s (OH / CCOO)

System has all parameters available.

This example shows that all models can be used to calculate activity coefficients.

3 Calculating Flash Points

The button “Calculate Flashpoint” will calculate the flash points for given composition. A dialog pops up where compositions can be entered:

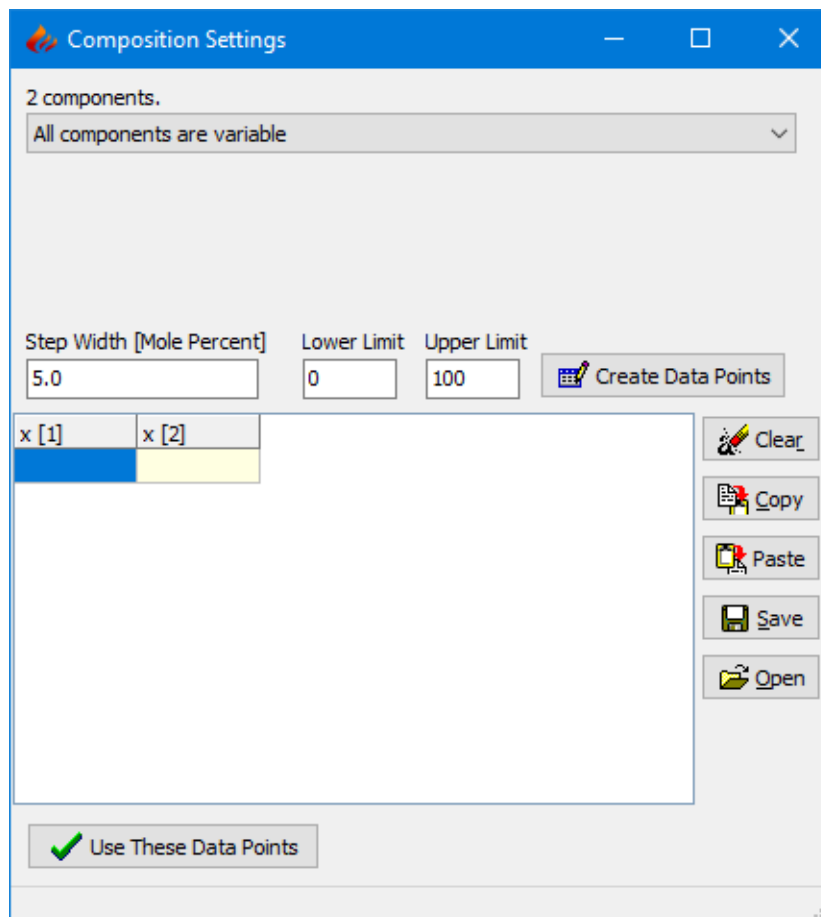


Figure 5: Composition

Wanted compositions can either be entered directly in the data grid or automatically created by the “Create Data Points” button.

For the automatic creation, it is possible to specify lower and upper limits of compositions and the step width. For mixture with three or more components it is possible to specify constant compositions or constant mole fraction ratios.

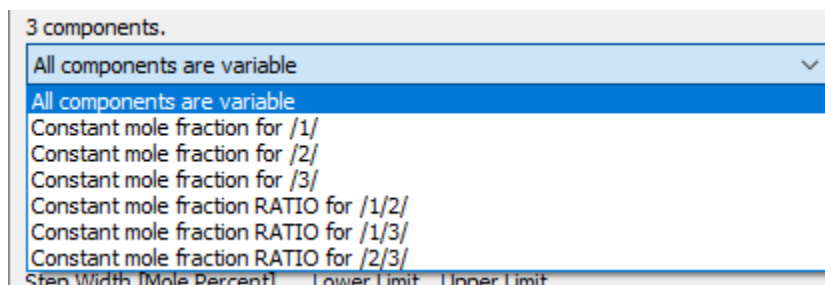


Figure 6: Options for the automatic data point creation.

The created data points will be displayed in the data grid

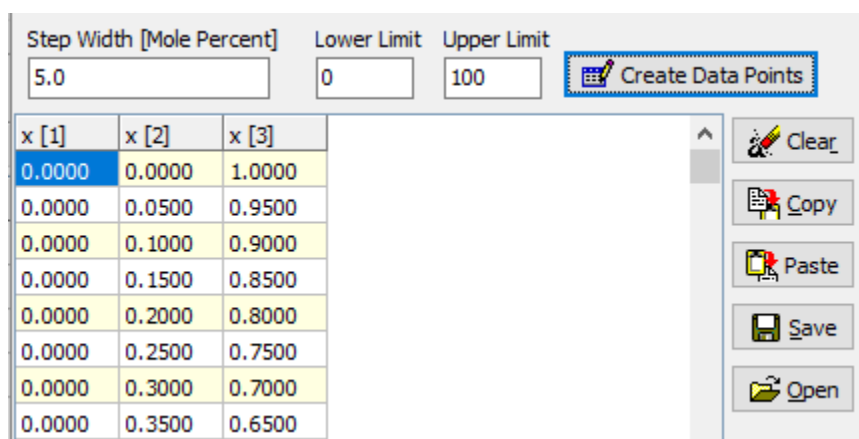


Figure 7: Automatically created compositions.

and can be copied to the Windows clipboard or saved as CSV files (Comma Separated Values). If data are available in other programs (like spread sheets) or on disk the data table can be pasted or loaded.

The “Use These Data Points” button closes this dialog and starts the calculation, the “Close” also closes this dialog but does not start the calculation (like “Cancel”).

3.1 Standard or Custom Compositions

Custom Compositions

It is possible to calculate just 21 points in 5 mole-% steps and without specifying the compositions manually by switching the option “Custom Compositions” off.

3.2 Calculation Result

The data grid contains three parts.

Result Table		Antoine Parameters	PURE.FLP			
x1 [mol/mol]	x2 [mol/mol]	T Flash Point [K]	Act.Coeff.1	Act.Coeff.2	wliq1 [g/g]	wliq2 [g/g]
0.00000	1.00000	285.927	2.55522	1.00000	0.00000	1.00000
0.11862	0.88138	287.784	2.22194	1.00931	0.05000	0.95000
0.22127	0.77873	289.398	1.96891	1.03544	0.10000	0.90000
0.31095	0.68905	290.701	1.77317	1.07661	0.15000	0.85000
0.38999	0.61001	291.857	1.61934	1.13196	0.20000	0.80000
0.46016	0.53984	292.923	1.49687	1.20125	0.25000	0.75000
0.52289	0.47711	293.838	1.39831	1.28474	0.30000	0.70000
0.57930	0.42070	294.699	1.31834	1.38308	0.35000	0.65000
0.63029	0.36971	295.578	1.25305	1.49725	0.40000	0.60000
0.67661	0.32339	296.400	1.19952	1.62861	0.45000	0.55000
0.71888	0.28112	297.271	1.15556	1.77885	0.50000	0.50000
0.75760	0.24240	298.080	1.11047	1.95012	0.55000	0.45000

The compositions are the composition either entered manually or created automatically. The flash point temperatures and the activity coefficients are calculated values.

The content of this data table can either be copied to the Windows clipboard or saved as Microsoft Excel 2007 files (extension “xls”).

3.3 Diagrams

Diagrams are available for binary and ternary mixtures. Typical results are shown in this chapter.

3.3.1 Ternary Mixtures

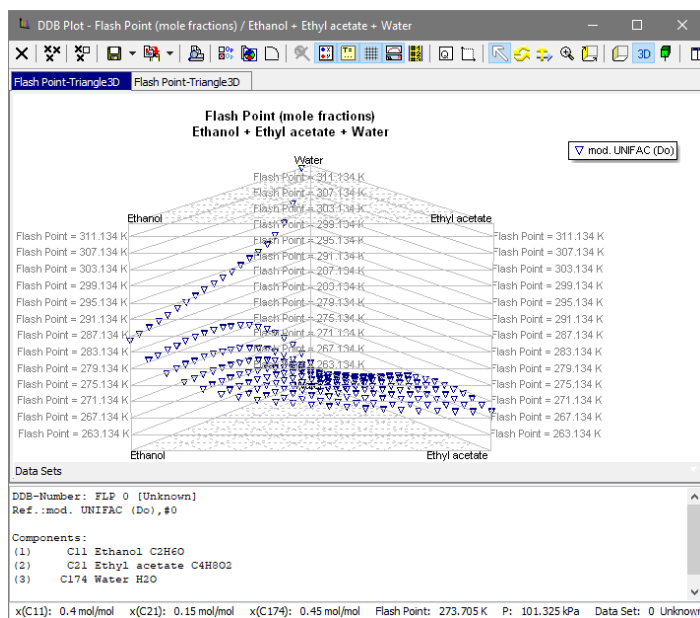


Figure 8: Flashpoint diagram of a ternary mixture.

3.3.2 Binary Mixtures

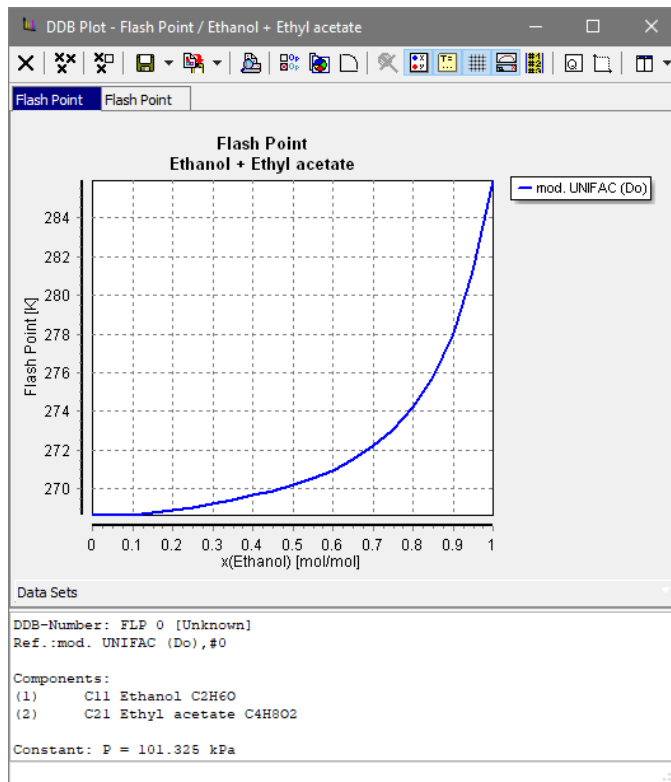


Figure 9: Flashpoint diagram of a binary mixture.

A description of the plot program is available separately ("DDBPlot.pdf").

3.4 LLE Calculation

The program allows the calculation of miscibility gaps (liquid-liquid equilibria) for binary mixtures only. If a LLE is found, no flash point is calculated and the compositions in the data grid are set to light red.

Result Table						
Antoine Parameters		PURE.FLP				
x1 [mol/mol]	x2 [mol/mol]	T Flash Point [K]	Act.Coeff.1	Act.Coeff.2	wliq1 [g/g]	wliq2 [g/g]
0.05000	0.95000	306.805	18.35521	1.02075	0.17800	0.82200
0.10000	0.90000	306.805	9.80100	1.07329	0.31373	0.68627
0.15000	0.85000	306.805	6.03535	1.14959	0.42065	0.57935
0.20000	0.80000	306.805	4.12635	1.24529	0.50705	0.49295
0.25000	0.75000	306.805	3.05490	1.35782	0.57832	0.42168
0.30000	0.70000	306.805	2.40521	1.48557	0.63812	0.36188
0.35000	0.65000	306.805	1.98705	1.62755	0.68900	0.31100
0.40000	0.60000	306.805	1.70518	1.78310	0.73283	0.26717
0.45000	0.55000	306.805	1.50828	1.95181	0.77098	0.22902
0.50000	0.50000	306.805	1.36699	2.13338	0.80448	0.19552
0.55000	0.45000	306.805	1.26360	2.32761	0.83413	0.16587
0.60000	0.40000	306.805	1.18698	2.53434	0.86056	0.13944
0.65000	0.35000	306.612	1.12985	2.75344	0.88427	0.11573
0.70000	0.30000	306.070	1.08728	2.98479	0.90566	0.09434
0.75000	0.25000	305.672	1.05587	3.22824	0.92506	0.07494

Figure 10: Result table with marked LLE.

In binary diagrams the LLE area is shown as a straight horizontal line:

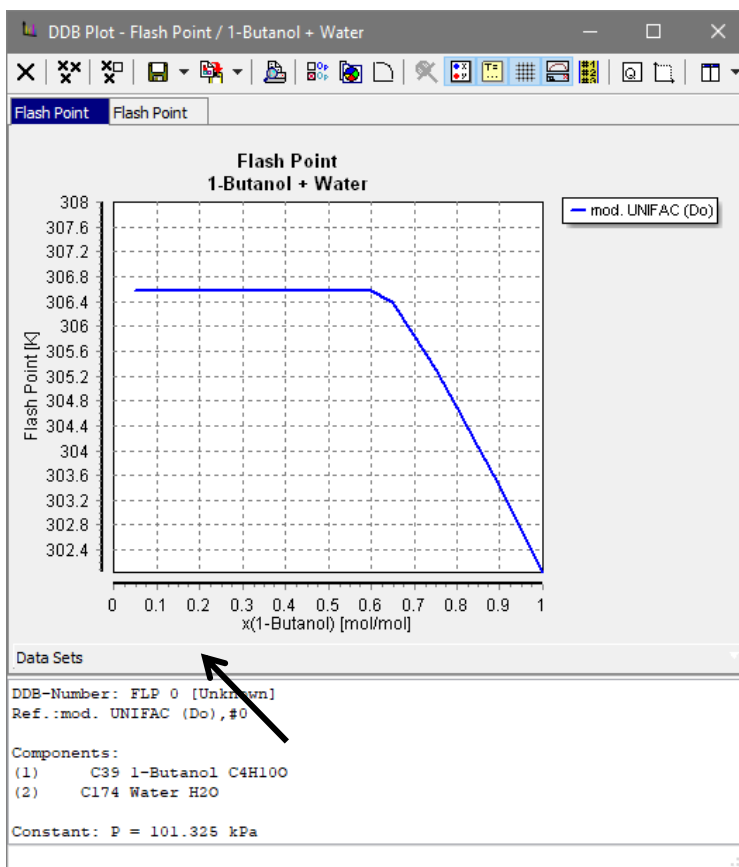


Figure 11: Plot of the calculation results.

The LLE is not determined exactly. Instead all given compositions are tested if they are inside the miscibility gap.