

## **Changes for DDBSP 2016 Update1**

*Release Date: November 30, 2016*

### **Basic Version / Mixture Prediction**

- New: support for Aspen V9.0 added

### **Artist / Basic Version / GC2gE / Mixture Calculation / RecPar**

- New [Aspen INP export]: allow selection of Aspen version to be used in the DATABANKS/PROP-SOURCES section

### **GC2gE / RecPar**

- Fixed \* *Regression in version 2016* \*: the Aspen parameters are displayed as "not compatible" if the DDB term  $dij \cdot T \cdot \ln(T)$  is not 0

### **Basic Version**

- Fixed [CompoundListEditor] \* *Regression in version 2016* \*: remove component(s) from a list does no longer work correctly
- Fixed [ComponentSelection]: the search by vapor pressure/boiling point does not work correctly if the local decimal point is not '.'
- Fixed [ComponentSelection] \* *Regression in version 2016* \*: the search by vapor pressure does no longer work correctly
- Fixed [ComponentSelection] \* *Regression in version 2016* \*: the displayed Antoine temperature range is wrong for negative values (°C)

### **Mixture Fit**

- Fixed [GenPar]: 2-phase flash calculation stops if ICP parameters are missing

### **Mixture Prediction**

- Fixed \* *Regression in version 2015* \*: VLE prediction text output does no longer use local decimal point

### **Predictive EOS**

- Fixed: PSRK/VTPR 3-phase flash gives wrong results, even in the 2-phase region

### **Process Synthesis**

- Fixed [EntrainerSelection]: finding components for azeotropic distillation doesn't work for a constant system pressure